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(54) **POLYOLEFIN POLYMER COMPOSITIONS COMPRISING GLYCEROL MONOESTERS OF C 20-24 FATTY ACIDS AND FOAMED ARTICLES PREPARED THEREFROM**

GLYCERIN-MONOESTER VON C20-24-FETTSÄUREN UMFASSENDE
POLYOLEFIN-POLYMERZUSAMMENSETZUNGEN UND GESCHÄUMTE ARTIKEL DARAUS
COMPOSITIONS POLYMERES D'OLEFINE COMPRENANT DES MONOESTERS DE GLYCEROL
D'ACIDES GRAS C 20-24 ET MOUSSES PREPAREES SELON LESDITES COMPOSITIONS

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EP-A- 0 229 882 FR-A- 2 411 853
US-A- 3 644 230

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Description

This invention relates to novel polyolefin compositions, to a process for making foamed or expanded articles therefrom and to foams of these polyolefin compositions which are characterized, in fresh or non-fully cured form, by improved elevated temperature distortion characteristics. In addition the foamed products prepared from the present compositions possess improved electrostatic dissipation properties.

It is common practice to make closed-cell ethylenic polymer foams by an extrusion foaming process comprising the steps of heat plastifying a thermoplastic ethylenic polymer; admixing the heat plastified polymer under pressure with a volatile material such as a chlorofluorocarbon and passing the resulting mixture through a die opening or shaping orifice into a zone of lower pressure to vaporize the volatile constituent and form a cellular structure which upon cooling forms the corresponding cellular solid ethylenic polymer foam. However, the development of a viable commercial extrusion foaming process--especially for relatively low density foams of lower polyolefin--requires balancing a number of different (and sometimes competing) business and technical requirements. Accordingly, much of the extrusion foaming technology is empirical, based upon experience and directed to very specific materials and processes to produce specific commercial products.

One of the requirements for acceptable polyolefin foam products of growing importance is the elevated temperature distortion characteristics of such products in fresh or partially cured form (that is, the dimensional stability at elevated temperature of the foam prior to sufficient storage or aging to permit substantially complete replacement of the original blowing agent within the cellular structure of the foam with air). Such characteristic is of growing importance because (a) the elevated temperature distortion characteristics of relatively fresh polyolefin foams are significantly dependent upon the particular ingredients (for example, blowing agent, additives, etc.) employed in its preparation; (b) warehousing costs, storage space factors, and/or other considerations oftentimes mandate shipment of the polyolefin foam products from the manufacturing facility prior to the time that they become fully cured; and (c) such partially cured foam products may, during transport in enclosed vehicles, particularly in warm climates or during hot weather, be subjected to prolonged exposure at relatively high temperatures. Moreover, this concern is even further aggravated by the recent trend toward the use of various stability control agents which provide improved ambient temperature dimensional stability with a wider variety of blowing agents, but which unfortunately also generally lengthen the time required for the polyolefin foam product to reach its so-called fully cured state.

Additionally, the industry has recently begun using so called "soft" chlorofluorocarbon blowing agents, in particular CFC-142b (1-chloro-1,1-difluoroethane), mixtures containing such soft chlorofluorocarbons or hydrocarbon blowing agents such as isobutane. These compounds have been found to be more readily converted in the environment to decomposition products having reduced deleterious effects. Disadvantageously CFC-142b and isobutane permeate faster through ethylenic polymers than air resulting in foam collapse. To avoid this problem it has become necessary to employ stability control agents to retard the permeation rate of these halocarbon or hydrocarbon blowing agents.

In U.S. Patent 4,368,276 suitable N-substituted fatty acid amides are disclosed for use in polyolefin foams as stability control agents. In certain end uses, such as packaging for sensitive electronic parts, foams must possess electrostatic dissipation properties to prevent an accumulated electrostatic charge on the foam surface from discharging through contact with the electronic part. Although operating effectively for many end uses, it has been discovered that foams prepared utilizing the foregoing N-substituted fatty acid amides do not show measurable improvement in electrostatic dissipation. Moreover, when static control agents such as alkyl amines are added to the formulation the stability control properties of the N-substituted fatty acid amide are adversely affected.

FR-A-2 411 853 discloses expandable polyolefin compositions comprising a polyolefin, a volatile organic blowing agent and a glycerol monoester of a C₂₀ fatty acid.

In view of the foregoing, it is an object of this invention to provide polyolefin foams having, in fresh foam form, good elevated temperature distortion properties as well as to provide polyolefin compositions which are expandable to form such improved polymer foams. Another object of this invention is to provide polyolefin foams having increased electrostatic dissipation properties. Other objects and advantages of the present invention will be apparent from the description thereof which follows.

The foregoing and related objectives are attained by the practice of the present invention which, in one aspect, is a polyolefin composition comprising a polyolefin and from about 0.1 to about 10 weight percent based upon the polyolefin of glycerol monoesters of C₂₀₋₂₄ fatty acids.

In another aspect, the present invention is the above-noted type of polyolefin composition which further comprises a volatile organic blowing agent and which is thereby expandable to form an expanded article (that is, a polymer foam) of said polyolefin composition.

Finally, a particularly beneficial aspect of the present invention resides in a method for substantially improving the elevated temperature distortion characteristics (for example, dimensional stability at elevated temperatures such as, for example, 66°C, the maximum heat distortion temperature, etc.) of relatively fresh polyolefin foams by incorporating therein (for example, during extrusion foaming thereof) from about 0.1 to about 10 weight percent, based upon the

polyolefin, of the above described fatty acid monoesters. The features of the present invention are particularly beneficial when practiced with a blowing agent comprising CFC-142b, or similar soft chlorofluorocarbon; isobutane, or similar hydrocarbon; or mixtures thereof.

Polyolefins suitable for use in the practice of the present invention include homopolymers of ethylene as well as copolymers thereof with other monomers such as propylene, butene-1, 1-octene and other olefins, especially α -olefins, (referred to as linear low density polyethylene); vinyl esters of saturated carboxylic acids such as vinyl acetate and vinyl propionate; alkyl esters of monoethylenically unsaturated carboxylic acids such as methyl acrylate or methacrylate, ethyl acrylate or methacrylate, propyl acrylate or methacrylate, the several butyl# and isobutyl acrylates and methacrylates. 2-ethylhexyl acrylate, dimethyl maleate; the various monoethylenically unsaturated carboxylic acids themselves such as, for example, acrylic acid, methacrylic acid, ethacrylic acid, crotonic acid, mesaconic acid. Polymers of particular interest for use herein are polyethylene, linear low density polyethylene, ethylene-vinyl acetate copolymers and ethylene-acrylic acid copolymers. Naturally, blends of 2 or more of the above-noted polyolefins can also be suitably employed.

As has been noted, a key feature of the present invention resides in the use of a small amount of a glycerol monoester of a C_{20-24} fatty acid wherein a glycerol monoester of a C_{20} fatty acid is excluded, in conjunction with the above-described polyolefin to provide polyolefin foams having, in fresh foam form improved distortion and stability characteristics at elevated temperatures. A preferred stability control agent is glycerol monobehenate.

The glycerol monoester may be present in mixture with other fatty acid esters depending on the purity of fatty acid used to manufacture the same. Typically, behenic acid is a hydrogenated rape seed oil containing by weight about 60 percent C_{22} fatty acids, 38 percent C_{18} fatty acids and 2 percent C_{16-14} fatty acids. In addition, as much as 40 percent by weight of the ester mixture may constitute diesters and 15 percent by weight triesters in the mixture.

In addition to the above-described fatty acid monoesters, there may also be employed, as auxiliary stability control agents, certain other compounds such as, for example, the higher alkyl amines, the fatty acid esters, the fatty acid amides or N-substituted fatty acid amides which are described in U.S. Pat. No. 4,214,054, U.S. Pat. No. 3,644,230 or U.S. Pat. No. 4,368,276. Such additives may be employed in order to obtain an advantageous balance of both ambient temperature and elevated temperature dimensional stability characteristics in the polyolefin foams prepared therewith.

Additionally, a static dissipation agent may be included in the present composition. Such antistatic agents include alkyl amines, ethoxylated alkyl amines, and alkenyl amines and quaternary ammonium compounds which surprisingly do not adversely affect the stability control properties of the present compositions. Other additives such as nucleation aids (for example, talcum powder, sodium bicarbonate, calcium silicate, etc.), colorants, antioxidants, etc. may also be included.

In the practice of the present invention, the above-described fatty acid monoesters are preferably employed in an amount of from 0.15 to 5 weight percent based upon the weight of the polyolefin. Moreover, regardless of whether the glycerol monoester of a C_{20-24} fatty acid is employed alone or in combination with the above-noted auxiliary stability control additives, the total level of such additives combined will typically not be in excess of 10 weight percent based upon the polyolefin weight and the minimum amount of the compound employed will preferably be an amount sufficient to prevent the fresh foam prepared therewith from shrinking more than 10 percent in volume during prolonged exposure at 66°C.

The expanded polyolefin articles of the present invention (also referred to herein as polyolefin foams) can be conveniently prepared using conventional extrusion foaming principles by heat plastifying the desired polyolefin resin and incorporating into such heat plastified polymer at elevated temperature and pressure (a) a volatile organic blowing agent and (b) from 0.1 to 10 weight percent (based upon the polyolefin) of the above-discussed fatty acid monoester (or a mixture of such ester with one or more of the above-noted auxiliary stability control agents) to form a flowable gel of an expandable polyolefin composition and thereafter extruding said gel into a zone of lower pressure and temperature to form the desired substantially closed-cell polyolefin foam.

The volatile organic blowing agent is compounded into the starting polyolefin resin in proportions suitable to provide the desired degree of expansion in the resulting foamed cellular product, usually up to a 100-fold volume expansion to make products having aged foam densities down to 9.6 kilograms per cubic meter (kg/m^3). Depending on the starting proportion of blowing agent, the resulting foam products of this invention will typically have densities in the range of from 9.6 to 160 kg/m^3 . Preferably, the foam products of the invention are of relatively low density (for example, in the range of from 16 to 96 kg/m^3 and the practice of such invention is especially beneficial for polyolefin foams having densities in the range of from 16 to 48 kg/m^3). Typically, the amount of volatile organic blowing agent employed in preparing polyolefin foams in such density ranges will be in the range of from 0.02 to 0.35 gram mole thereof per 100 grams of the polyolefin employed.

The choice of the specific volatile organic blowing agent selected for use in the present invention is not particularly critical. Indeed, it is a particularly beneficial aspect of the instant invention that the use of the above-described fatty acid monoesters (or their mixtures with the above-noted auxiliary stability control agents) facilitates obtaining of low density polyolefin foams having commercially desirable properties (for example, ambient temperature dimensional

stability and/or suitable fresh foam elevated temperature distortion characteristics, etc.) with a much broader range of volatile organic blowing agent systems than was heretofore possible. Such volatile organic blowing agents can suitably be employed in the practice of the present invention either alone or in conjunction with thermally decomposable gas-releasing chemical blowing agents or auxiliary blowing agents such as water, carbon dioxide, etc., though such auxiliary blowing agents are also useful as blowing agents by themselves or as primary blowing agents. Preferably, volatile organic blowing agents are employed which have an atmospheric boiling point below the melting point of the polyolefin employed.

Representative of suitable volatile blowing agents include halogenated hydrocarbon compounds having from 1 to 4 carbon atoms (for example, trichlorofluoromethane, dichlorodifluoromethane, dichlorofluoromethane, chlorodifluoromethane, 1,1,2-trichlorotrifluoroethane, 1,2-dichlorotetrafluoroethane, 1,1-dichloro-2,2,2-trifluoroethane, 1,1-dichloro-1-fluoroethane, 1-chloro-1,2,2,2-tetrafluoroethane, 1-chloro-1,1-difluoroethane, 1,1,1,2-tetrafluoroethane, 1,1-difluoroethane, ethyl chloride, methyl chloride, methylene chloride, etc.) as well as volatile non-halogenated hydrocarbon compounds such as propane, butane, isobutane, butene, propylene, pentane, etc. Naturally, mixtures of two or more of the foregoing blowing agents can also be suitably employed and, indeed, an especially preferred embodiment of the present invention involves the use of a mixed blowing agent system comprising from 40 to 90 weight percent of 1-chloro-1,1-difluoroethane and from 60 to 10 weight percent of ethyl chloride, both weight percentages being based upon the total weight of such mixed blowing agent system.

As has been noted, the blowing agent is compounded into the starting polyolefin in conventional fashion to make a flowable gel, preferably in a continuous manner, for example, in a mixing extruder, using heat to plastify the normally solid polymer, pressure to maintain the blowing agent in non-gaseous state, and mechanical working to obtain a thorough mixing of the polymer and blowing agent. The resulting gel is then cooled if necessary and passed through a suitable die orifice into a zone of lower pressure, for example, normal ambient air pressure, where it expands to a lower density, cellular mass. As the extruded product foams, it is taken away from the extruder, allowed to cool to harden the resulting polymer foam and collected for further processing, storage and use.

The resulting polyolefin foam is comprised of substantially closed-cell structure and, even at low densities, that is, from 16 to 48 kg/m³ and when in fresh foam form, is remarkably stable in dimension at ambient temperature as well as upon exposure to elevated temperatures.

For the present purposes, the dimensional stability of the extrusion foamed products is measured by observing the changes in volume occurring in test specimens of the foam as a function of time of exposure under the environmental circumstances of concern. The test specimens are obtained by quickly cutting, from the extrusion foamed product soon, for example, within about fifteen minutes, after emerging from the extrusion die orifice, test pieces of the desired dimensions (conveniently, samples 13 cm long, 1.3 cm thick and 2.5 cm wide can be suitably employed) and accurately measuring their overall volume, for example, by cubic displacement of water. The initial volume of each specimen is arbitrarily selected as the benchmark volume for the subsequent dimensional stability study.

For ambient temperature dimensional stability testing, the individual foam specimens are exposed to air at atmospheric pressure and ordinary room temperature (for example, 23°C) and their volumes are measured periodically to determine the minimum volume to which they shrink during the ambient temperature curing process (that is, "curing" referring to the phenomenon in which the gaseous blowing agent within the foam cells is gradually diffusing out thereof and during which air is gradually diffusing in to replace the escaping blowing agent). For elevated temperature dimensional stability performance evaluation, the above-described ambient temperature procedures are followed except that the specimen is exposed to atmospheric pressure air at elevated temperatures rather than at ambient temperature. The polymer foams of the present invention preferably do not shrink by more than 20 percent and more preferably not more than from 15 percent from their original volume (measured 5 minutes after extrusion) after two weeks of aging under either ambient (for example, 23°C) or elevated temperature (ambient to 160°C) test conditions.

In addition, another test employed herein is evaluation of the static dissipating properties of the foam. Test methods include measuring both the surface resistivity (ASTM D-257) and static decay time (Federal Test Standard 101C Method 4046.1).

The specific working examples that follow are intended to illustrate the invention but are not to be taken as limiting its scope. In the examples, parts and percentages are by weight unless otherwise specified or required by the context.

Example 1

The equipment used in this example is a 2.54 cm (1") screw type extruder having additional zones for mixing and cooling at the end of sequential zones for feeding, metering and mixing. An opening for blowing agent addition is provided on the extruder barrel between the metering and mixing zones. At the end of cooling zone, there is attached a die orifice having an opening of rectangular shape. The height of the opening, hereinafter called die gap, is adjustable while its width is fixed at 3.68 mm.

One hundred parts of granular low density polyethylene (2.1 melt index, 0.923 g/cc density) was uniformly blended

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with 2.0 parts of glycerol monobehenate (Kemaster 6500, Humko Chemical Div.) in concentrate form and 0.25 parts of talcum powder. The blend was fed into the extruder at a uniform rate of approximately 6 pounds per hour (2.7 kg/hr). The temperatures maintained at the extruder zones were 95°C at the feeding zone, 150°C at the melting zone, 180°C at the metering zone and 200°C at the mixing zone. CFC-142b (1-chloro-1,1-difluoroethane) was injected under pressure into the mixing zone at a predetermined rate to produce foam of the desired density. The temperature of the cooling zone was maintained so that the polymer/blowing agent mixture could reach an optimum foaming temperature which was in the range of 106°C ± 1°C. The die gap was adjusted in each test to provide a foam strand having smooth skin.

At a die gap ranging from 0.9 mm to 1.1 mm, there were saved foam samples for determination of foam dimensional stability. The foam strands were of oval shape with approximately 1.1 cm x 1.6 cm dimensions and cell sizes ranging from about 0.45 mm to 0.85 mm. From the strand, four 12.7 cm long pieces of foam specimens were cut out and their initial weight and volume were measured within about 5 minutes. Two pieces were aged at ambient temperature and one piece each at 54°C and 71°C, respectively. The weight and volume of the foam specimens were periodically determined, hourly for the first 6 hours and daily for the first week and then weekly.

The comparative samples were prepared in a similar manner excepting that no stability control agent was added to the polymer melt.

As the data summarized in Table I show, glycerol monobehenate provides foam dimensional stability at temperatures as high as 71°C.

Table I

Run	Foam Density ¹	Foam Dimensional Stability ²		
		Ambient Temp.	(54°C)	(71°C)
1	32	91	95	95
*	41	72	ND	ND

*Not an example of this invention

ND = Not determined

¹ Density of cured foam body in kilograms per cubic meter measured two months after extrusion.

² Minimum volume of foam body as a percentage of the initial (measured 5 minutes after extrusion) during 2 week aging at specified temperatures.

Example 2

The same apparatus, temperature settings, polymer type, stability control agent amount, talc level and solid feed rate as used in Example 1 were employed in the tests of this example. In Run 3, 1 percent by weight of an alkyl amine type antistatic agent (Atmer 163 made by ICI Americas) was included. The blowing agent was selected from CFC-142b or its mixture (55/45 mole ratio) with ethyl chloride (Run 4). The blowing agent was fed at a uniform rate of approximately 0.15 gram moles per 100 grams of polymer throughout the tests of this example. Die openings, foam cross-section sizes and cell sizes fell approximately in the same ranges as for the tests of Example 1.

The test results summarized in Table II indicate that 2.0 parts of glycerol monobehenate per hundred parts of polyethylene together with 1 pph (parts per hundred) Atmer 163 provides adequate static dissipating properties without loss of foam dimensional stability. Advantageously, glycerol monobehenate alone without addition of an antistatic agent, imparts a measurable static dissipating property to the foam. In terms of static decay time per Federal Test Standard 101C method 4046.1, all the foams meet the requirement of the test.

Table II

Run	Blowing Agent Type ¹	Antistatic Agent Level ² (pph)	Foam Dimensional Stability ³		Surface Resistivity ⁴	Static Decay Time ⁵
			Ambient Temp.	(54°C)		
2	CFC-142b	-	91	95	47.0	1.9
3	CFC-142b	1	95	102	3.9	0.65

¹ Atmer 163 brand antistatic agent (an alkyl amine type made by ICI Americas Inc.) mixed in per hundred parts of polymer

² Atmer 163 brand antistatic agent (an alkyl amine type made by ICI Americas Inc.) mixed in per hundred parts of polymer

³ minimum volume of foam body as a percentage of the initial (measured 5 minutes after extrusion) during aging at specified temperatures

⁴ Surface resistivity in 1012 ohms per square determined per ASTM D-257

⁵ Static decay time in seconds determined per Federal Test Standard 101C Method 4046.1.

Table II (continued)

Run	Blowing Agent Type ¹	Antistatic Agent Level ² (pph)	Foam Dimensional Stability ³		Surface Resistivity ⁴	Static Decay Time ⁵
			Ambient Temp.	(54°C)		
4	CFC-142b/ EtCl:55/45	-	93	86	24.0	1.5

¹ CFC-142b = 1-chloro-1,1-difluoroethane

CFC-142b/EtCl:55/45 = 55/45 molar mixture of CFC-142b and ethyl chloride

² Atmer 163 brand antistatic agent (an alkyl amine type made by ICI Americas Inc.) mixed in per hundred parts of polymer³ minimum volume of foam body as a percentage of the initial (measured 5 minutes after extrusion) during aging at specified temperatures⁴ Surface resistivity in 1012 ohms per square determined per ASTM D-257⁵ Static decay time in seconds determined per Federal Test Standard 101C Method 4046.1.**Example 3**

Substantially the same resin blend as employed in Example 1 is extruded and foamed by means of a 1 1/2" (3.81 cm) screw type extruder having essentially the same configuration as the equipment used in Example 1 operating at substantially the same extrusion conditions. There is attached a die orifice having a rectangular opening of 6.35 mm x 1.27 mm.

One hundred parts of the low density polyethylene resin were blended with 1.4 parts of glycerol monobenhenate and 0.35 parts of a nucleating agent mixture, (a mixture of-sodium bicarbonate and citric acid in polyethylene, Hydrocerol® CF-20, available from Boehringer Ingelheim). The blend was fed into the extruder at a uniform rate of 4.5 kilograms per hour. Isobutane was injected into the extruder at a rate of (0.84 pounds) 3.8 kilograms per hour. At the foaming gel temperature of 110°C, there was achieved a good quality foam having 33 kg/m³ density, 1.5 mm cell size and 1 cm x 3.2 cm cross-section. From the foam strand, 10 cm long pieces were cut and subjected to similar dimensional stability tests as in the Example 1.

The data summarized in Table III indicate that glycerol monobenhenate provides desired dimensional stability for a polyethylene foam expanded with isobutane blowing agent.

Table III

Run	Foam Density ¹	Foam Dimensional Stability ²		
		Ambient Temp.	(66°C)	(71°C)
6	33	98	94	89

¹ Density of cured foam body in kilograms per cubic meter measured 7 days after extrusion.² The same as in Table I.**Claims**

1. A process for preparing a substantially closed-cell polyolefin foam having improved dimensional stability, characterized by (a) heat plastifying the polyolefin, (b) incorporating, into the heat-plastified polyolefin a glycerol monoester of a C₂₀₋₂₄ fatty acid, wherein a glycerol monoester of a C₂₀ fatty acid is excluded, in an amount from 0.1 to 10 weight percent based upon the polyolefin weight, (c) incorporating a volatile organic blowing agent in an amount from 0.02 to 0.35 gram-mole per 100 grams of polyolefin composition, and (d) thereafter extruding the formed flowable gel into a zone of lower pressure to thereby form said substantially closed-cell polyolefin foam.
2. The process of Claim 1, being further characterized in that the foam maintains at least 80 percent of its original volume after two weeks of aging at ambient temperature.
3. The process of Claim 1, being further characterized that the foam maintains at least 85 percent of its original volume after two weeks of aging at ambient temperature.
4. A closed-cell polyolefin foam obtainable by the process of any of the preceding claims.
5. An expandable polyolefin composition including a polyolefin and a volatile organic blowing agent capable of being

expanded to form a polyolefin foam having improved dimensional stability characterized in that the composition contains from 0.1 to 10 weight percent based upon the weight of said polyolefin of glycerol monoester of a C₂₀₋₂₄ fatty acid, wherein a glycerol monoester of a C₂₀ fatty acid is excluded.

6. The process, foam, or expandable composition according to any of the preceding claims, wherein the volatile blowing agent is isobutane.
7. The process, foam, or expandable composition according to any of the preceding claims wherein the fatty acid ester is glycerol monobehenate.
8. The process, foam, or expandable composition according to any of the preceding claims wherein the polyolefin is polyethylene.

Patentansprüche

1. Verfahren zur Herstellung eines im wesentlichen geschlossenzelligen Polyolefinschaums mit verbesserter Dimensionsstabilität, gekennzeichnet durch (a) Hitzeplastifizieren des Polyolefins, (b) Eingeben eines Glycerinmonoesters einer C₂₀₋₂₄-Fettsäure, wobei ein Glycerinmonoester einer C₂₀-Fettsäure ausgeschlossen ist, in das hitzeplastifizierte Polyolefin in einer Menge von 0,1 bis 10 Gew.-%, bezogen auf Polyolefingewicht, (c) Eingeben eines flüchtigen organischen Blähmittels in einer Menge von 0,02 bis 0,35 Gramm-Mol pro 100 Gramm von Polyolefinzusammensetzung und (d) danach Extrudieren des gebildeten fließfähigen Gels in eine Zone von niedrigerem Druck, um hierdurch diesen im wesentlichen geschlossenzelligen Polyolefinschaum zu bilden.
2. Verfahren nach Anspruch 1, weiter dadurch gekennzeichnet, daß der Schaum wenigstens 80 % seines ursprünglichen Volumens nach Alterung von zwei Wochen bei Umgebungstemperatur beibehält.
3. Verfahren nach Anspruch 1, weiter dadurch gekennzeichnet, daß der Schaum wenigstens 85 % seines ursprünglichen Volumens nach Alterung von zwei Wochen bei Umgebungstemperatur beibehält.
4. Geschlossenzelliger Polyolefinschaum, erhältlich nach dem Verfahren eines der vorherigen Ansprüche.
5. Expandierbare Polyolefinzusammensetzung, einschließlich ein Polyolefin und ein flüchtiges organisches Blähmittel und fähig unter Bildung eines Polyolefinschaums mit verbesserter Dimensionsstabilität expandiert zu werden, dadurch gekennzeichnet, daß die Zusammensetzung von 0,1 bis 10 Gew.-%, bezogen auf das Gewicht dieses Polyolefins, eines Glycerinmonoesters einer C₂₀₋₂₄-Fettsäure, wobei ein Glycerinmonoester einer C₂₀-Fettsäure ausgeschlossen ist, enthält.
6. Das Verfahren, der Schaum oder die expandierbare Zusammensetzung nach einem der vorhergehenden Ansprüche, worin das flüchtige Blähmittel Isobutan ist.
7. Das Verfahren, der Schaum oder die expandierbare Zusammensetzung nach einem der vorhergehenden Ansprüche, worin der Fettsäureester Glycerinmonobehenat ist.
8. Das Verfahren, der Schaum oder die expandierbare Zusammensetzung nach einem der vorhergehenden Ansprüche, worin das Polyolefin Polyethylen ist.

Revendications

1. Procédé de préparation d'une mousse de polyoléfine à alvéoles pratiquement fermées, présentant une stabilité dimensionnelle améliorée, caractérisé en ce que
 - (a) on plastifie à chaud la polyoléfine,
 - (b) on incorpore dans la polyoléfine plastifiée à chaud un monoester de glycérol d'un acide gras en C₂₀₋₂₄, à l'exclusion d'un monoester de glycérol d'un acide gras en C₂₀, en une quantité représentant de 0,1 à 10 % en poids par rapport au poids de la polyoléfine,
 - (c) on y incorpore un agent d'expansion organique volatil, en une quantité de 0,02 à 0,35 mole pour 100

grammes de la composition de polyoléfine, et

(d) on extrude ensuite le gel fluide formé, dans une zone où règne une pression plus faible, pour former ainsi ladite mousse de polyoléfine à alvéoles pratiquement fermées.

- 5 2. Procédé conforme à la revendication 1, caractérisé en outre en ce que la mousse conserve au moins 80 % de son volume initial après deux semaines de vieillissement à la température ambiante.
3. Procédé conforme à la revendication 1, caractérisé en outre en ce que la mousse conserve au moins 85 % de son volume initial après deux semaines de vieillissement à la température ambiante.
- 10 4. Mousse de polyoléfine à alvéoles fermées, que l'on peut obtenir selon un procédé conforme à l'une des revendications précédentes.
- 15 5. Composition de polyoléfine expansible, qui contient une polyoléfine et un agent d'expansion organique volatil, et qui peut être expansée pour donner une mousse de polyoléfine présentant une stabilité dimensionnelle améliorée, ladite composition étant caractérisée en ce qu'elle contient de 0,1 à 10 % en poids, par rapport au poids de ladite polyoléfine, d'un monoester de glycérol et d'un acide gras en C₂₀₋₂₄, à l'exclusion d'un monoester de glycérol et d'un acide gras en C₂₀.
- 20 6. Procédé, mousse ou composition expansible, conforme à l'une quelconque des revendications précédentes, dans lequel ou laquelle l'agent d'expansion volatil est de l'isobutane.
7. Procédé, mousse ou composition expansible, conforme à l'une quelconque des revendications précédentes, dans lequel ou laquelle l'ester d'acide gras est du monobéhénate de glycérol.
- 25 8. Procédé, mousse ou composition expansible, conforme à l'une quelconque des revendications précédentes, dans lequel ou laquelle la polyoléfine est un polyéthylène.

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